

From last time

$$c(z) \rho(z) \frac{\partial u(x, t)}{\partial t} = \frac{\partial}{\partial x} \left(k_0(z) \frac{\partial u}{\partial x} \right) + Q(x, t)$$

General heat equation for a 1-D conducting rod.

Heat equation that we study:

$$c(z) \rho(z) \frac{\partial u(x, t)}{\partial t} = k_0 \frac{\partial^2 u(x, t)}{\partial x^2}$$

Even simpler assume $c=c(x)$ and $\rho=\rho(x)$ are also const.

$$c \rho \frac{\partial u(x, t)}{\partial t} = k_0 \frac{\partial^2 u(x, t)}{\partial x^2}$$

Thus

$$\boxed{\frac{\partial u}{\partial t} = k \frac{\partial^2 u}{\partial x^2}}$$

$$\text{where } k = \frac{k_0}{c \rho}.$$

A → simplest heat equation.

diffusivity
rate of diffusion of the heat.

Conducting rod



• physically need to know what happens at the ends of the domain.. $x=0$ and $x=L$

• what was the initial temperature distribution in the rod,

Physical units in this problem

$$\frac{\partial u}{\partial t} = k \frac{\partial^2 u}{\partial x^2}$$

$$\frac{\partial u}{\partial t} \sim \frac{[u]}{[T]}$$

$$\frac{\partial^2 u}{\partial x^2} \sim \frac{[u]}{[L]^2}$$

$$k \sim \frac{[u]}{[T]}$$

$$\frac{[u]}{[L]^2} = \frac{[L]^2}{[T]}$$

diffusivity
rate of diffusion of the reactant

$$k = \frac{k_0}{c_p} =$$

$$\frac{[E]}{[M][L][u]} = \frac{[M][u]}{[L]^3} =$$

dimensional consistency
as these are the same...

What are the dimensions of k_0 ?

$$\phi(x, t) \approx -k_0(x) \frac{\partial u}{\partial x}$$

$$\phi \sim \frac{[E]}{[T][L]^2}$$

$$\frac{[E]}{[T][L]^2} = [k_0] \frac{[u]}{[L]}$$

$$k_0 \sim \frac{[E]}{[T][L]^2} \cdot \frac{[u]}{[L]} = \frac{[E]}{[T][L][u]}$$

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- The PDE $\frac{\partial u}{\partial t} = k \frac{\partial^2 u}{\partial x^2}$

- The initial conditions.
- The boundary condition

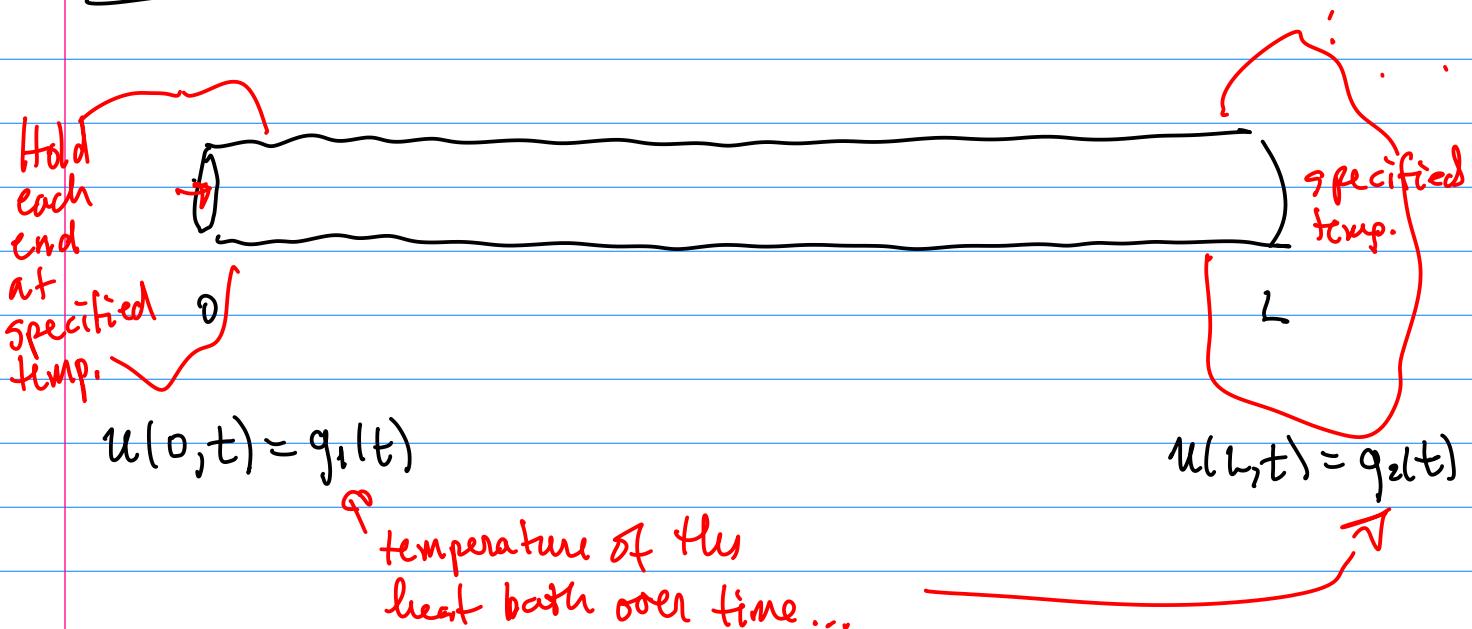
Initial conditions: specify the distribution of heat

for example, $u(x, 0) = f(x)$ for $x \in [0, L]$

initial distribution of heat

Boundary Condition:

Heat Bath:



Insulated boundary condition. No flux at the boundary

$$q(0, t) = 0 \quad \text{and} \quad q(L, t) = 0$$



No flux of heat energy through the boundary.

Since

$$q(x, t) = -k_b(x) \frac{\partial u}{\partial x}$$

$$0 = q(0, t) = -k_b(0) \frac{\partial u}{\partial x} \Big|_{x=0} = 0$$

$$x=0$$

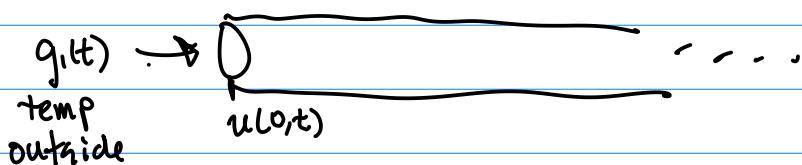
$$\text{thus } \frac{\partial u}{\partial x} \Big|_{x=0} = 0$$

In terms of temperature insulated boundary conditions.

$$\left. \frac{\partial u}{\partial x} \right|_{x=0} = 0, \quad \left. \frac{\partial u}{\partial x} \right|_{x=L} = 0$$

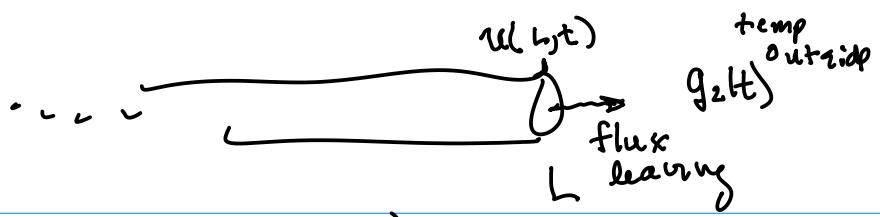
Newton's law of Cooling

(and rod temperatures). Experiments show that, as a good approximation, the heat flow leaving the rod is proportional to the temperature difference between the bar and the prescribed external temperature. This boundary condition is called **Newton's law of cooling**. If it is valid at $x = 0$, then



$$\sim k_b \left. \frac{\partial u}{\partial x} \right|_{x=0} = q_i(t) = H_1 (q_i(t) - u(0, t))$$

$$x=0$$



$$-K_0 \frac{\partial u}{\partial x} \Big|_{x=L} = q(L, t) = H_2(u(L, t) - q_2(t))$$

Goal: predict the future.

Simpler Goal: predict superfar into the future
as $t \rightarrow \infty$.

Idea: as $t \rightarrow \infty$ the heat distribution enters into an equilibrium state provided none of the boundary terms have an explicitly time dependence.,,

For example the heat bath ..

$$\begin{aligned} u(0, t) &= q_1(t) & u(L, t) &= q_2(t) \\ q_1 & \uparrow & q_2 & \uparrow \\ \text{temp at} & & \text{temp at} & \\ \text{left } t & & \text{right } t & \end{aligned}$$

$$\begin{aligned} q_1(t) &= q_1 \\ q_2(t) &= q_2 \\ u(0, t) &= q_1 & \xrightarrow{\text{constant infinite}} & u(L, t) = q_2 \end{aligned}$$

If in equilibrium then $\frac{\partial u}{\partial t} = 0$ so the heat equation reduces to

$$0 = K \frac{\partial^2 u}{\partial t^2}$$

Solve this next time: